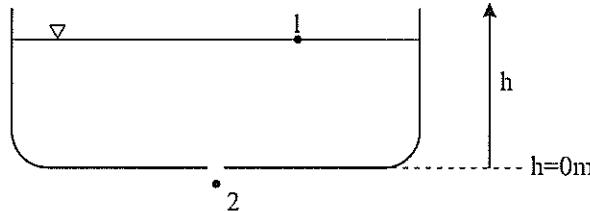


Free outflow from vessel

Velocity of outflow



Point 2 is somewhat lower than the hole, here the streamlines are already parallel, but this height difference can be neglected.

$$\frac{v_1^2 \cdot \rho}{2} + h_1 \cdot \rho \cdot g + p_1 = \frac{v_2^2 \cdot \rho}{2} + h_2 \cdot \rho \cdot g + p_2 + f \cdot \frac{L_{\text{total}}}{D_e} \cdot \frac{v_2^2 \cdot \rho}{2}$$

$p_1 = p_2$ (the pressure difference of the air due to height can be neglected)

$v_1 \approx 0 \text{ m/s}$ because the vessel is much wider than the hole

$f = 0, L_{\text{total}} = 0 \text{ m}$

$$h_1 \cdot \rho \cdot g = \frac{v_2^2 \cdot \rho}{2} + h_2 \cdot \rho \cdot g$$

$$\frac{v_2^2 \cdot \rho}{2} = (h_1 - h_2) \cdot \rho \cdot g$$

$$v_2 = \sqrt{2 \cdot g \cdot (h_1 - h_2)} = \sqrt{2 \cdot g \cdot h}$$

Flow rate of outflow

$$\dot{V} = A_{\text{hole}} v_2 = \frac{D_e^2 \pi}{4} \sqrt{2 \cdot g \cdot h}$$

Time of outflow

Differential equation of the change of volume in time

$$dV = -\dot{V} \cdot dt$$

$$A_{\text{vessel}} \cdot dh = -\alpha \cdot A_{\text{hole}} \cdot v \cdot dt$$

$$A_{\text{vessel}} \cdot dh = -\alpha \cdot A_{\text{hole}} \cdot \sqrt{2 \cdot g \cdot h} \cdot dt$$

$$\frac{A_{\text{vessel}}}{-\alpha \cdot A_{\text{hole}}} \cdot \frac{1}{\sqrt{2 \cdot g}} \cdot \frac{1}{\sqrt{h}} dh = dt$$

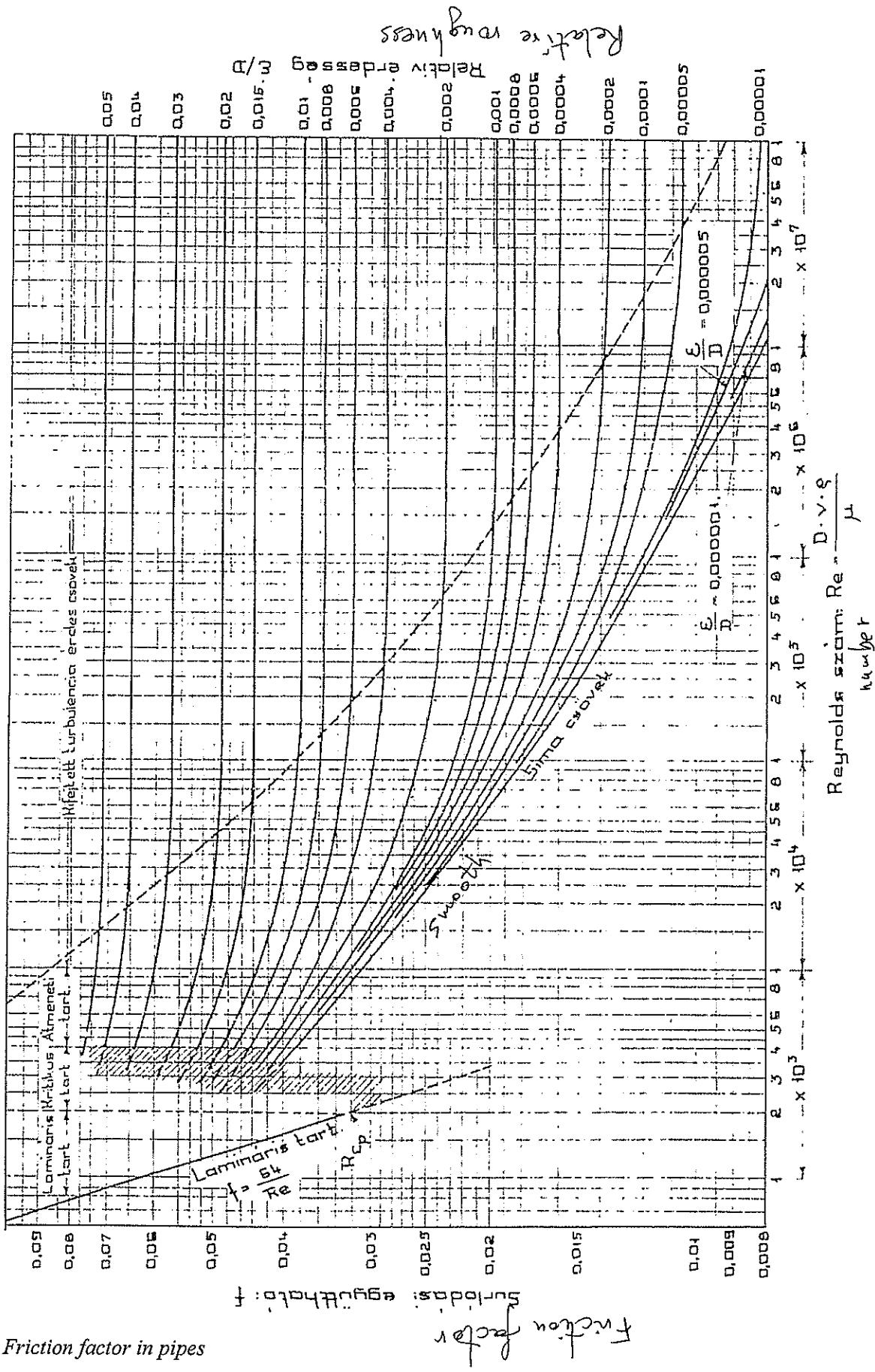
where α is a so-called outflow factor expressing what fraction is utilized due to turbulence.

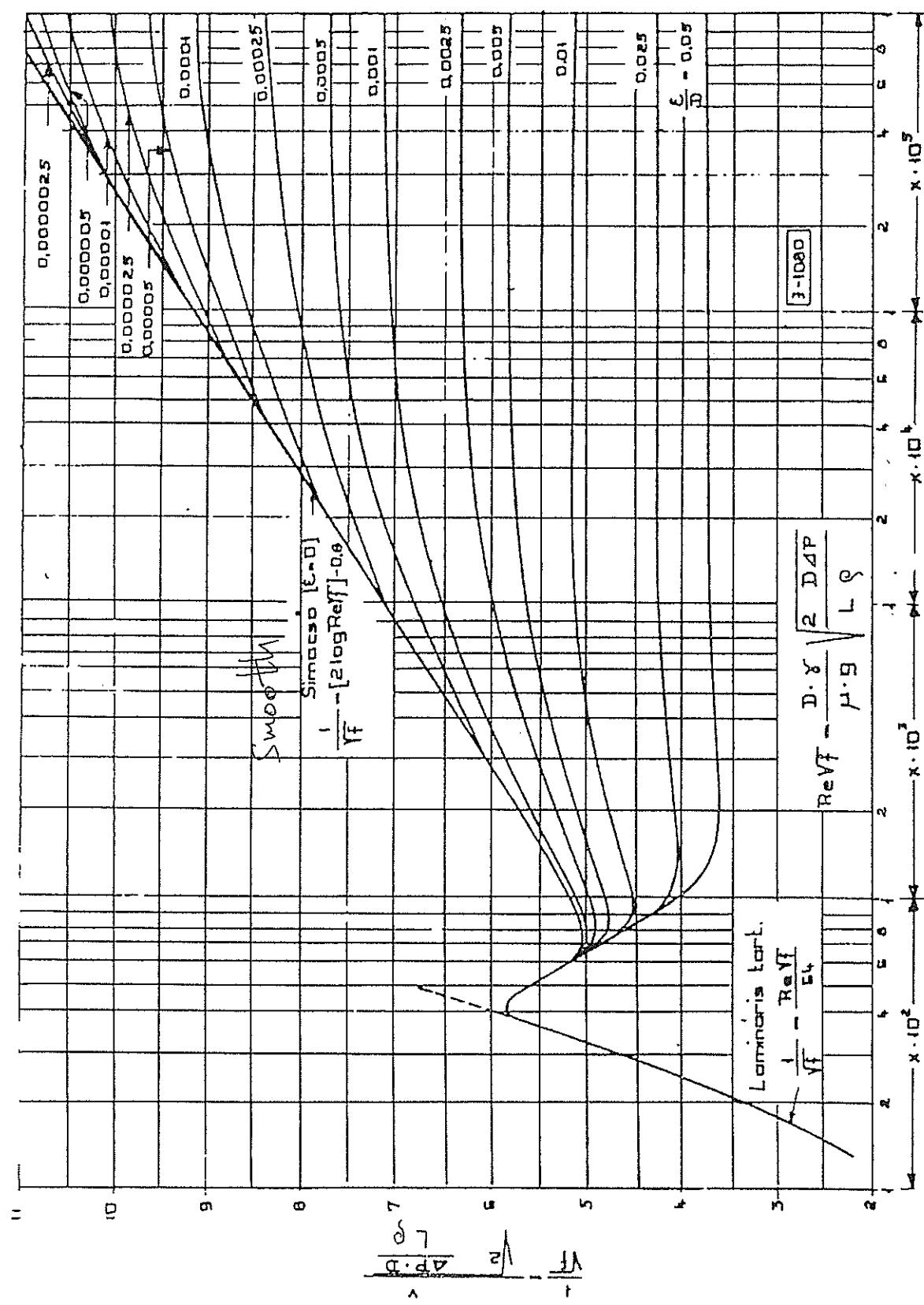
Solution:

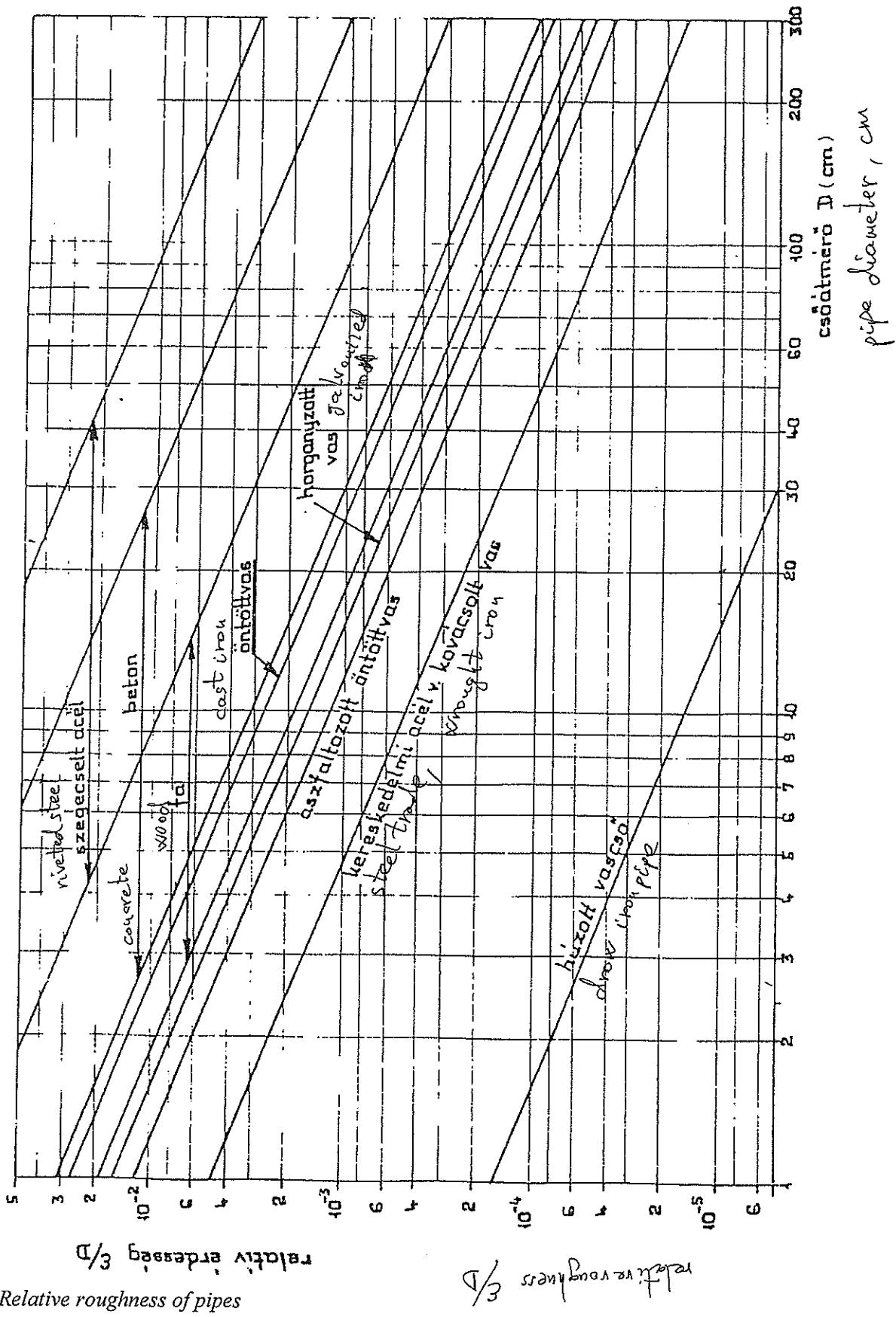
$$t = \frac{2 \cdot A_{\text{vessel}}}{\alpha \cdot A_{\text{hole}} \cdot \sqrt{2 \cdot g}} \cdot (\sqrt{h_0} - \sqrt{h_1}) \quad h_0 > h_1$$

This is the time decreasing the level from h_0 to h_1 .

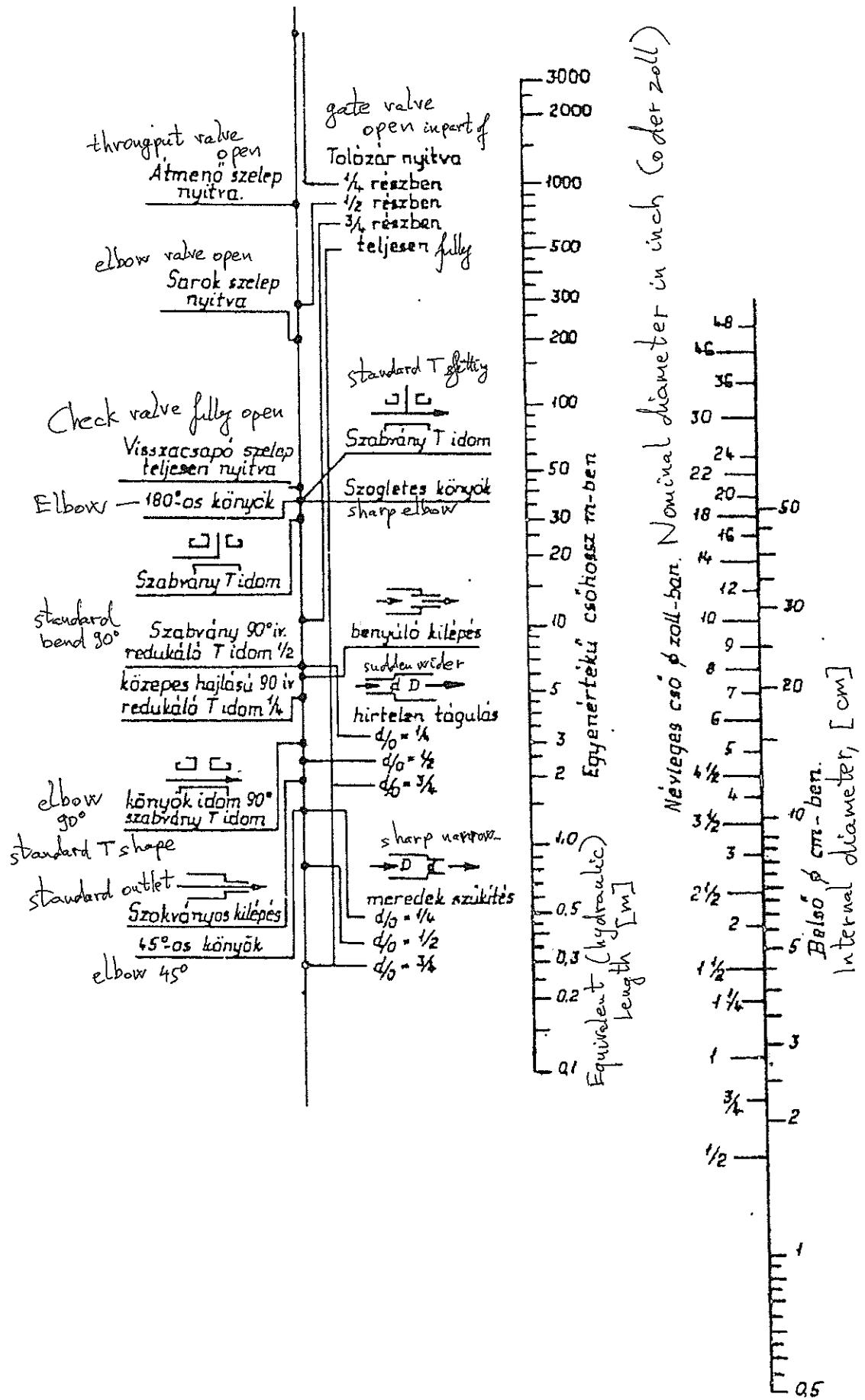
$h = 0 \text{ m}$ must be the height where the level can decrease to (perhaps during infinite time).







Relative roughness of pipes



Equivalent pipe length nomogram